

Cooperative CO₂ Absorption Isotherms from a Bifunctional Guanidine and Bifunctional Alcohol

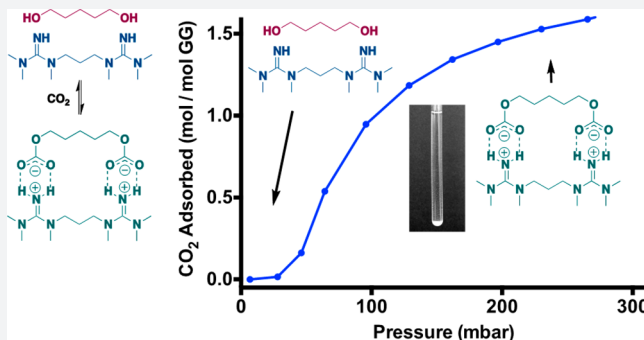
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S Supporting Information

ABSTRACT: Designing new liquids for CO₂ absorption is a challenge in CO₂ removal. Here, achieving low regeneration energies while keeping high selectivity and large capacity are current challenges. Recent cooperative metal–organic frameworks have shown the potential to address many of these challenges. However, many absorbent systems and designs rely on liquid capture agents. We present herein a liquid absorption system which exhibits cooperative CO₂ absorption isotherms. Upon introduction, CO₂ uptake is initially suppressed, followed by an abrupt increase in absorption. The liquid consists of a bifunctional guanidine and bifunctional alcohol, which, when dissolved in bis(2-methoxyethyl) ether, forms a secondary viscous phase within seconds in response to increases in CO₂. The precipitation of this second viscous phase drives CO₂ absorption from the gas phase. The isotherm of the bifunctional system differs starkly from the analogous monofunctional system, which exhibits limited CO₂ uptake across the same pressure range. In our system, CO₂ absorption is strongly solvent dependent. In DMSO, both systems exhibit hyperbolic isotherms and no precipitation occurs. Subsequent ¹H NMR experiments confirmed the formation of distinct alkylcarbonate species having either one or two molecules of CO₂ bound. The solvent and structure relationships derived from these results can be used to tailor new liquid absorption systems to the conditions of a given CO₂ separation process.



Large-scale CO₂ capture has been proposed as an important—and perhaps necessary—tool for limiting atmospheric CO₂ concentrations.¹ A number of commercial projects currently employ aqueous monoethanolamine or other liquid amine systems to separate CO₂ from other gases, including for natural gas processing or postcombustion capture.² Significant energy is required to desorb the CO₂, adding operational costs that have limited wider deployment of CO₂ capture technology.^{3,4}

Chemists have developed a wide array of materials aimed at reducing the energy required for CO₂ capture.^{5,6} Such materials include ionic liquids,^{7,8} metal–organic frameworks,^{9,10} and other sorbents.^{11–15} These materials typically have hyperbolic isotherms where CO₂ uptake increases quickly at lower pressures, but levels off as available binding sites become saturated. This type of thermodynamic behavior presents a fundamental dichotomy: materials exhibiting high CO₂ affinity are often correspondingly difficult to desorb, while materials exhibiting low affinity may show poor CO₂ uptake or lack selectivity for CO₂ over other gases.

One strategy for overcoming this dichotomy is to design a material that transitions between high and low affinity binding. In the high affinity regime, the material would bind CO₂ strongly and selectively; in the low affinity regime, the CO₂

would readily desorb. This is commonly seen in nature, where hemoglobin uses this method to capture and release O₂. Cooperative diamine-functionalized metal organic frameworks use steric and amine affinity to tune this transition from low to high affinity,¹³ potentially improving the efficiency of CO₂ capture by allowing absorption/desorption cycles to occur over a narrower pressure or temperature range.¹⁴ In another example, the Schneider and Brennecke groups reported an ionic liquid that melts upon CO₂ binding, exhibiting sigmoidal isotherms.¹⁵ The associated heat of fusion (ΔH_{fus}) contributes to the heat required for CO₂ desorption. Still, examples of cooperative CO₂ absorption isotherms remain scarce. New strategies for obtaining cooperative isotherms would provide a valuable resource to design more efficient CO₂ capture materials.

Herein, we report a solution phase system comprising a bidentate guanidine (GG) and bidentate alcohol (AA) that exhibits cooperative isotherms at ambient temperature (Figure 1). Solution-based methods for CO₂ capture are of great interest, due, in part, to the possibility of incorporation within monoethanolamine CO₂ binding infrastructure.

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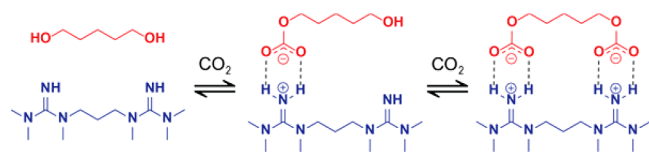
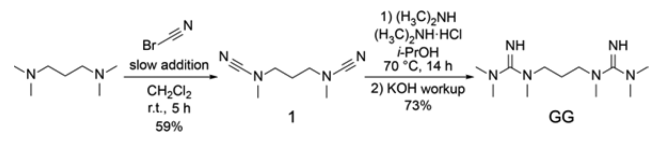


Figure 1. CO₂ binding by a bidentate alcohol and bidentate guanidine. A solution of 1,5-pentandiol (AA) and bis(trimethylguanidine) species (GG) may capture CO₂ in a cooperative fashion.

The 1,1'-(propane-1,3-diyl)bis(1,3,3-trimethylguanidine) (GG) 1,5-pentandiol (AA) system extends chemistry developed by Jessop, Heldebrandt, and co-workers^{16–18} in which an alcohol and strong organic base react with CO₂. The reaction forms the salt of a negatively charged alkyl carbonate species and a positively charged, protonated base. We hypothesized that, for a bifunctional system, binding of the first CO₂ molecule would generate an ionic interaction that facilitates binding of the second CO₂ molecule (Figure 1).

We measured CO₂ absorption isotherms for the system comprising the bifunctional guanidine shown in Figure 1 (GG) and a commercially available bifunctional alcohol (1,5-pentandiol, AA). The bifunctional guanidine GG was synthesized in two steps on multigram scale. First, 1,3-bis(dimethylamino)propane was reacted with cyanogen bromide to afford bis-cyanamide **1**.^{19,20} Next, the bis-cyanamide was reacted with dimethylamine and dimethylamine·HCl to obtain the corresponding bis-guanidinium dichloride, which was treated with concentrated aqueous KOH to obtain 1,1'-(propane-1,3-diyl)bis(1,3,3-trimethylguanidine), GG (Scheme 1; see Supporting Information for details).

Scheme 1. Synthesis of Bifunctional Guanidine GG



To determine the potential for these bidentate species to exhibit cooperative isotherms, we conducted analysis on a gas sorption analyzer adjusted for a liquid system (3-Flex). (The physical dissolution of CO₂ in the solvent was measured independently and subtracted from the overall absorption to determine the chemically absorbed component. Additionally, an approximation of the initial flask volume was used due to the liquid phase of the analytes. See Supporting Information section II, p 16, for complete details.) In early experiments, we observed that solvent plays a large role in controlling CO₂ binding for the AA:GG system. Specifically, in bis(2-methoxyethyl) ether (diglyme) we observed an increased amount of CO₂ absorbed overall vs DMSO, as well as an inflection point—a transition from low affinity to high affinity—in the shape of the CO₂ absorption isotherm. We calculated a Hill coefficient of 2.4 for this isotherm, indicating cooperative binding of CO₂.²¹ For measures of the CO₂ binding capacities of other system components, please see Table S2.

After observing the unique responses of the AA:GG system in diglyme, we sought to determine how the solvent was influencing binding. We examined an analogous monodentate CO₂ binding system to see how solvent related to CO₂-binding ability (Figure 2a). Analysis of the slope of the isotherm did not

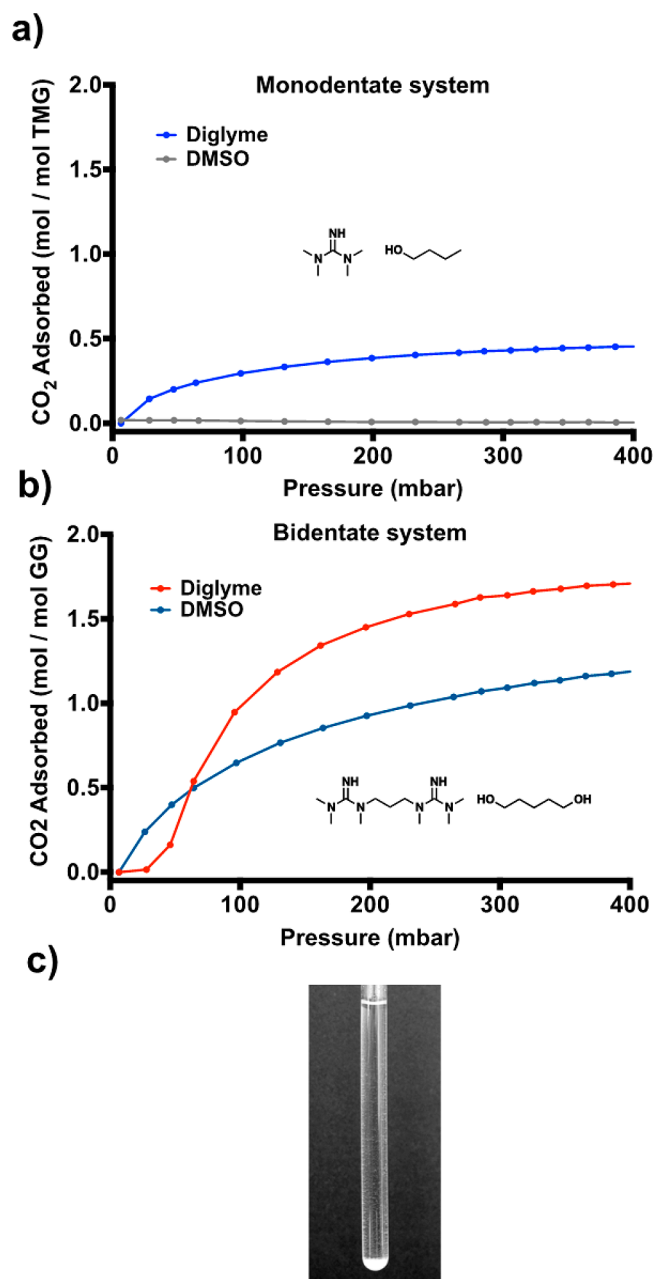


Figure 2. CO₂ absorption isotherms varying solvent and denticity. (a) 50 mM GG and 75 mM AA in diglyme and DMSO at 22 °C. (b) 50 mM *N,N,N',N'*-tetramethylguanidine and 75 mM *n*-butanol in DMSO and bis(2-methoxyethyl) ether at 22 °C. (c) An NMR sample of a CO₂-saturated mixture of GG:AA, 1:1 ratio, evolves a viscous secondary phase (see Supporting Information section III for further details).

suggest a shift in CO₂ binding between low and high pressure regimes, and no precipitation was observed. It should be noted that, relative to the bidentate GG AA system, CO₂ absorption is suppressed across the entire isotherm.

The altered shape of the AA:GG binding isotherm in diglyme relative to the monodentate suggested potential cooperativity in the bidentate system, as evidenced by the appearance of distinct low affinity and high affinity CO₂ binding regimes. (Figure 2a,b). This transition was always accompanied by the precipitation of a second phase from the CO₂ capture solution. This may explain, in part, why diglyme demonstrates a dramatic

CO₂ absorption transition, whereas DMSO does not: the precipitation of the second phase (which contains CO₂) correlates with the binding mode change (Figure 2c). The selection of diglyme as a medium for CO₂ absorption agrees with solvent surveys reported for CO₂ capture with monoethanolamine.²²

With a functional solvent determined, we next sought to ascertain the correct molar ratio of GG to AA to provide optimized CO₂ absorption (Figure 3a). In an interesting relationship, we found that 1:1 GG:AA displayed low affinity up to 68 mbar, where it sharply transitions to high affinity behavior. CO₂ absorption plateaus at approximately 1.1 mol/

mol GG. In stark contrast, a relatively small change in ratio, 1:1.5 GG:AA, results in a very different isotherm. Here, low affinity behavior begins to transition earlier, at approximately 29 mbar, and CO₂ absorption levels at approximately 1.7 mol/mol GG. Increasing the ratio further does very little to change the CO₂ absorption profile: 1:2 GG:AA transitions to high affinity at 28 mbar, and CO₂ absorption levels at approximately 1.8 mol/mol GG. These data reinforce the hypothesis of the bimolecular requirement for CO₂ binding.

We next determined if concentration of GG:AA in diglyme would change the binding properties by potentially increasing the cooperativity and therefore the transition point (Figure 3b). A ratio of 10 mM GG to 15 mM AA resulted in a suppressed isotherm compared to higher concentrations, with an affinity switch occurring at 166 mbar. A ratio of 100 mM GG:150 mM AA resulted in a decreased pressure range of low affinity behavior, and a leveling off of CO₂ absorption at approximately 1.4 mol/mol GG, indicating some suppression of high affinity behavior relative to the 50 mM GG:75 mM AA regime. The Hill coefficient remained 2.4. This suppression may be due to the viscosity of the CO₂-rich phase prohibiting successful mixing with a magnetic stirring apparatus. In light of these results, 50 mM AA:75 mM AA was used for all further experiments.

As we had observed the formation of a distinct second phase, we hypothesized that the solubility of the second phase may be an important factor in determining the onset of the precipitation and the low to high affinity transition. To test this, we examined absorption as a function of solution temperatures (Figure 3c). We observed a striking temperature dependence on the cooperative CO₂ binding of our system. At 11 °C, a region of suppressed uptake—low CO₂ affinity—is not observed at the pressure regime assayed, though this does not preclude its existence. Conversely, at 30 °C the region of low affinity extends until 101 mbar, almost three times the pressure at which the shift to high affinity occurs at 22 °C. This results in a change in the capacity of ~0.06 mmol of CO₂ per mL of liquid at 165 mbar. While modest, this represents a large change in the overall capacity of 70% at a target CO₂ pressure over a very modest temperature range.

At all temperatures and concentrations assayed, the inflection in the CO₂ absorption isotherm, corresponding to the transition from low affinity to high affinity, coincided with visually observable precipitation of a second, viscous phase. This phase appeared to contain predominantly A⁺A⁺G⁺G⁺-2 (CO₂) and led us to hypothesize that the captured CO₂ was precipitating. To clarify, we sought further characterization.

The precipitated phase was a highly viscous, turbid liquid (Figure 2c, Figure S9) that could be removed from the vial and analyzed, but would dissipate upon dissolution in other solvents, such as DMSO. ATR-IR analysis of the precipitate (Figure S7) showed that the phase was composed predominantly of alkylcarbonate and guanidinium functional groups, formed from the reaction of AA and GG with CO₂. These data indicate that there is limited solubility of the bis-alkylcarbonate and bis-guanidinium species, resulting in the formation of the new, CO₂-rich phase.

The ATR-IR data, as well as the suppression in CO₂ uptake, is consistent with previous observations by Heldebrandt and co-workers that nonpolar solvents trigger CO₂ desorption by destabilizing the charged alkylcarbonate and guanidinium species.¹⁷ Unlike the monofunctional system, bifunctional AA and GG appear to gain CO₂ affinity as correlating with the

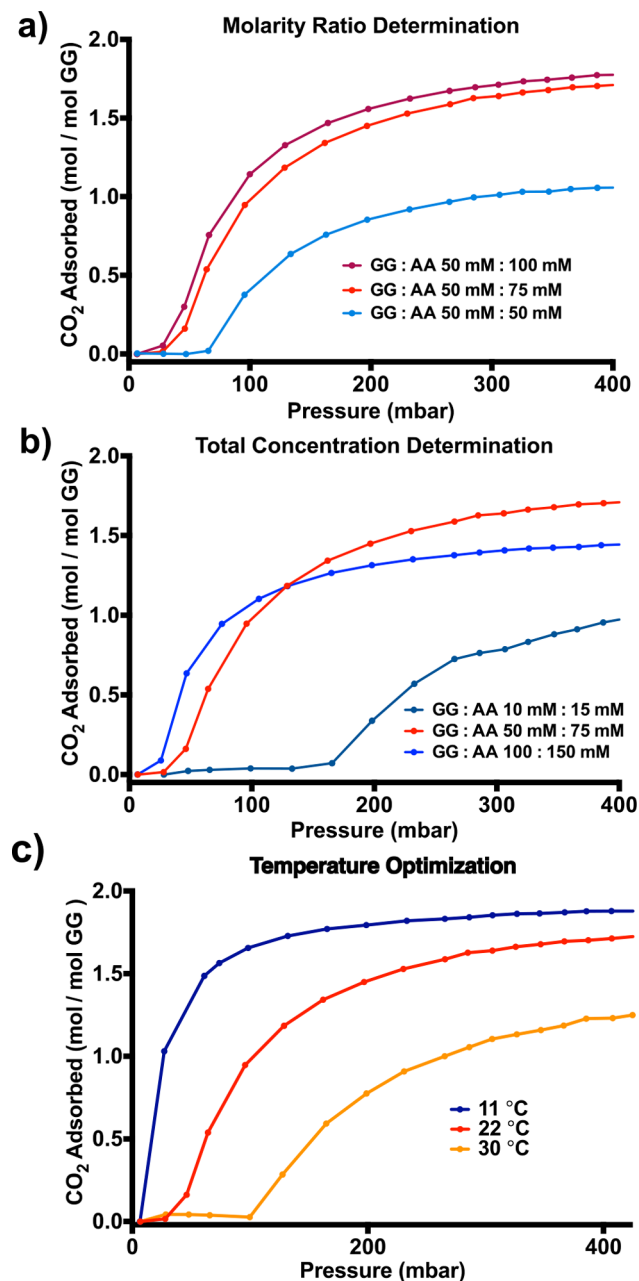


Figure 3. Evaluation of CO₂ absorption parameters. (a) Optimization of molar ratios of GG to AA in diglyme at 22 °C. (b) Optimization of concentrations of a 1:1.5 molar ratio of GG to AA in diglyme at 22 °C. (c) Temperature optimization of a 1:1.5 molar ratio of GG:AA in diglyme.

precipitation process. We hypothesize that the affinity is caused by two interrelated factors: (1) the linker couples binding of the first and second CO₂ molecules, so that the binding of the first molecules facilitates the second equivalent; (2) the resulting bis-cationic and bis-anionic species have relatively low solubility in diglyme. As increasing concentrations of CO₂ increase the concentration of the charged species, the charged species precipitate after reaching a solubility limit, designated by the temperature and solvent.

Based on these data, we can further understand the results seen in Figure 2. We hypothesize that DMSO, a strongly polar solvent, disrupts ion pairing between the cationic guanidinium and anionic alkylcarbonate functional groups of AAGG complex. Therefore, the charged functional groups remain dissociated and the binding of the first CO₂ molecule poorly facilitates binding of the second CO₂ molecule. DMSO disrupts other ionic interactions, especially by coordinating cations.^{23,24} Alternatively, DMSO may act as a better solvent for the AAGG complex, altering the equilibria associated with the CO₂ absorption process.

To further confirm whether the cooperative binding observed was the result of a cooperative phenomenon between the AA and GG species, we used ¹H NMR to study CO₂ binding by AA and GG. For practical reasons, we used a cosolvent mixture of DMSO-*d*₆ and acetonitrile-*d*₃ to prepare NMR samples. A minimum of 20% (v/v) DMSO-*d*₆ was required to maintain a homogeneous solution, so samples were prepared ranging from 20 to 100% DMSO-*d*₆.

Exposure of solutions containing AA and GG to 1 atm of CO₂ led to the formation of two distinct alkylcarbonate species, mono-alkylcarbonate A[−]A and bis-alkylcarbonate A[−]A[−] (Figure 4a). These species possess well-resolved resonances in the $\delta = 3.6$ –3.9 ppm region corresponding to protons adjacent to the newly formed alkylcarbonate functional groups (H_b and H_d). The species assignments were confirmed by ¹H TOCSY and ¹³C NMR experiments (Supporting Information section III). To confirm our shift assignments, we synthesized phenyl carbonate analogues of A[−]A and A[−]A[−]; the ¹H NMR spectra of these isolable analogues resemble closely that of the CO₂-bound species. We also observed unreacted diol, meaning that all three species (AA, A[−]A, and A[−]A[−]) were present simultaneously. Additionally, signals corresponding to the bifunctional guanidine GG all shift downfield (Figure 4, dashed lines), indicating the formation of guanidinium species. (Unlike the alkyl carbonate species, distinct signals from these guanidinium species likely coalesce due to acid–base exchange between guanidine and guanidinium functional groups occurring much faster than the NMR time scale. Therefore, our assignment of mono-guanidinium and bis-guanidinium species by ¹H NMR remains putative.)

Supporting the hypothesis of cooperativity, we found that the relative concentrations of mono-alkylcarbonate A[−]A and bis-alkylcarbonate A[−]A[−] vary as a function of solvent composition, as well as the concentration of unreacted diol, [AA]_f (Figure 4c). The ratio of bis-alkylcarbonate to mono-alkylcarbonate ([A[−]A[−]]/[A[−]A]) reflects their relative stability in solution, which we quantified via integration of H_d and H_b. The ratio increases as the proportion of DMSO-*d*₆ decreases (Figure 4d, blue circles). Moreover, the ratio diverges from what would be expected if CO₂ binding were statistically determined, that is, if the linkage had no influence on whether diol AA binds one or two CO₂ molecules. The stability of the bis-alkylcarbonate thus increases relative to the mono-alkylcarbonate at lower DMSO

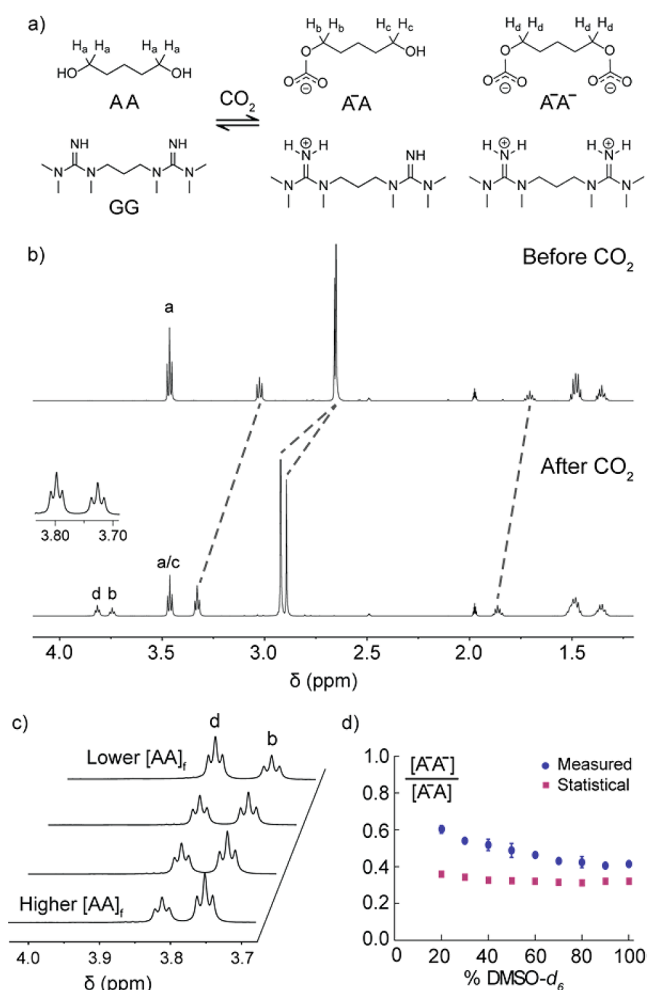


Figure 4. NMR analysis of CO₂ binding. (a) Species formed by AA and GG after exposure to 1 atm of CO₂. (b) ¹H NMR spectra before and after exposure to 1 atm of CO₂. Dashed lines correspond to GG or resulting guanidinium species. (c) Change in relative peak areas of H_b and H_d, which depend on solvent composition and final diol concentration, the latter shown. (d) Ratio of bis-alkylcarbonate A[−]A[−] to mono-alkylcarbonate A[−]A versus solvent composition.

concentrations. This is consistent with our previous hypothesis that DMSO disrupts the ionic interaction between anionic alkylcarbonate and cationic guanidinium functional groups.

One common method to quantify the proximity advantage, or chelate effect, is to calculate the effective molarity (EM) of one binding partner with respect to the other.²⁵ We performed additional ¹H NMR experiments in which [AA]_f was varied, and found that EM increases steadily as % DMSO-*d*₆ decreases, again suggesting that lower DMSO concentrations promote a stronger ionic interaction, agreeing with the bulk results observed in the isotherm as well as strongly supporting a cooperative mechanism (Figure S11).

In summary, we examined CO₂ binding by a system comprising a bifunctional guanidine and bifunctional alcohol. The system exhibits cooperative isotherms in diglyme, where CO₂ uptake is initially suppressed, but increases abruptly, with a corresponding precipitation of a viscous, CO₂-rich phase. The unique isotherm likely results from coordination between binding sites, and the limited solubility of bis-cationic and bis-anionic species formed. ¹H NMR studies confirmed that distinct mono-alkylcarbonate and bis-alkylcarbonate species are

formed upon CO₂ binding. Lower DMSO-*d*₆ concentrations favor the bis-alkylcarbonate and suggest that a tighter initial ionic interaction promotes binding of the second CO₂ molecule. This, to our knowledge, represents the first description of a liquid with cooperative CO₂ binding. Two of the advantages of a cooperative technology are that (1) the affinity shift of an improved cooperative system would facilitate less energy-intensive absorption/desorption, a known challenge for existing CO₂ binding systems, and (2) the liquid nature of the system is compatible with existing infrastructure. This system further shows that the cooperative gas binding observed in biologically optimized systems may be mimicked chemically with properties distinct from other CO₂ binding liquids and found only in a handful of solid materials.

■ ASSOCIATED CONTENT

Supporting Information

The Supporting Information is available free of charge on the ACS Publications website at DOI: [10.1021/acscentsci.7b00418](https://doi.org/10.1021/acscentsci.7b00418).

Details regarding synthesis, isotherm measurements, thermodynamic model, and NMR experiments (PDF)

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Notes

The authors declare no competing financial interest.

■ REFERENCES

- (1) International Energy Agency. *20 Years of Carbon Capture and Storage*; IEA Publications: Paris, 2016.
- (2) Rochelle, G. T. Amine Scrubbing for CO₂ Capture. *Science* **2009**, *325*, 1652–1654.
- (3) Rubin, E. S.; Davison, J. E.; Herzog, H. J. The Cost of CO₂ Capture and Storage. *Int. J. Greenhouse Gas Control* **2015**, *40*, 378–400.
- (4) Rubin, E. S.; Mantripragada, H.; Marks, A.; Versteeg, P.; Kitchin, J. The Outlook for Improved Carbon Capture Technology. *Prog. Energy Combust. Sci.* **2012**, *38*, 630–671.
- (5) D'Alessandro, D. M.; Smit, B.; Long, J. R. Carbon Dioxide Capture: Prospects for New Materials. *Angew. Chem., Int. Ed.* **2010**, *49*, 6058–6082.
- (6) Samanta, A.; Zhao, A.; Shimizu, G. K. H.; Sarkar, P.; Gupta, R. Post-Combustion CO₂ Capture Using Solid Sorbents: A Review. *Ind. Eng. Chem. Res.* **2012**, *51*, 1438–1463.
- (7) Seo, S.; et al. Chemically Tunable Ionic Liquids with Aprotic Heterocyclic Anion (AHA) for CO₂ Capture. *C. J. Phys. Chem. B* **2014**, *118*, 5740–5751.
- (8) Feng, Z.; et al. Absorption of CO₂ in the Aqueous Solutions of Functionalized Ionic Liquids and MDEA. *Chem. Eng. J.* **2010**, *160*, 691–697.
- (9) Nugent, P.; et al. Porous Materials with Optimal Adsorption Thermodynamics. *Nature* **2013**, *495*, 80–84.
- (10) Demessence, A.; D'Alessandro, D. M.; Foo, M. L.; Long, J. R. Strong CO₂ Binding in a Water-Stable, Triazolate-Bridged Metal-Organic Framework Functionalized with Ethylenediamine. *J. Am. Chem. Soc.* **2009**, *131*, 8784–8786.
- (11) Dawson, R.; Adams, D. J.; Cooper, A. I. Chemical Tuning of CO₂ Sorption in Robust Nanoporous Organic Polymers. *Chem. Sci.* **2011**, *2*, 1173–1177.
- (12) Walton, K. S.; Abney, M. B.; LeVan, M. D. Adsorption of CO₂ in Y and X Zeolites Modified by Alkali Metal Cation Exchange. *Microporous Mesoporous Mater.* **2006**, *91*, 78–84.
- (13) Mc Donald, T. M.; et al. Cooperative Insertion of CO₂ in Diamine-Appended Metal-Organic Frameworks. *Nature* **2015**, *519*, 303–308.
- (14) Siegelman, R. L.; et al. Controlling Cooperative CO₂ Adsorption in Diamine-Appended Mg₂(dobpdc) Metal-Organic Frameworks. *J. Am. Chem. Soc.* **2017**, *139*, 10526–10538.
- (15) Gurkan, B. E.; de la Fuente, J. C.; Mindrup, E. M.; Ficke, L. E.; Goodrich, B. F.; Price, E. A.; Schneider, W. F.; Brennecke, J. F. Equimolar CO₂ Absorption by Anion-Functionalized Ionic Liquids. *J. Am. Chem. Soc.* **2010**, *132*, 2116–2117.
- (16) Heldebrandt, D. J.; Yonker, C. R.; Jessop, P. G. Organic Liquid CO₂ Capture Agents with High Gravimetric CO₂ Capacity. *Energy Environ. Sci.* **2008**, *1*, 487–493.
- (17) Mathias, P. M.; et al. Improving the Regeneration of CO₂-Binding Organic Liquids with a Polarity Change. *Energy Environ. Sci.* **2013**, *6*, 2233–2242.
- (18) Koech, P. K.; et al. Low Viscosity Alkanolguanidine and Alkanolamidine Liquids for CO₂ Capture. *RSC Adv.* **2013**, *3*, 566–572.
- (19) Braun, J. v. Die Aufspaltung cyclischer Basen durch Bromcyan. *Ber. Dtsch. Chem. Ges.* **1907**, *40*, 3914–3933.
- (20) Hageman, H. A. The von Braun Cyanogen Bromide Reaction. *Org. React.* **1953**, *7*, 198–262.
- (21) Weiss, J. N. The Hill Equation Revisited: Uses and Misuses. *FASEB J.* **1997**, *11*, 835–841.
- (22) Huang, W.; Mi, Y.; Li, Y.; Zheng, D. An Apolar Protic Solvent, Diglyme, Combined with Monethanolamine to Form CO₂ Capture Material: Solubility Measurement, Model Correlation, and Effect Evaluation. *Ind. Eng. Chem. Res.* **2015**, *54*, 3430–3437.
- (23) Exner, J. H.; Steiner, E. C. Solvation and Ion Paring of Alkali-Metal Alkoxides in Dimethyl Sulfoxide. Conductometric Studies. *J. Am. Chem. Soc.* **1974**, *96*, 1782–1787.
- (24) Dijkstra, G.; Kruizinga, W. H.; Kellogg, R. M. An Assessment of the Causes of the "Cesium Effect". *J. Org. Chem.* **1987**, *52*, 4230–4234.
- (25) Hunter, C. A.; Anderson, H. L. What is Cooperativity? *Angew. Chem., Int. Ed.* **2009**, *48*, 7488–7499.