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# 1 **Biological Bromate Reduction Driven by Methane in a Membrane Biofilm Reactor**

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8

## 9 **Abstract**

10 As a potent greenhouse gas with a greenhouse warming potential 28 times that of carbon  
11 dioxide over a 100-year timescale, methane has been proven to be utilized as electron donor  
12 to remove various of contaminants, e.g. nitrate, nitrite, perchlorate, and chromate from  
13 contaminated water. However, microbial bromate reduction supported by methane has not  
14 been reported so far. Here, a lab-scale membrane biofilm reactor (MBfR) was set up to  
15 explore the feasibility of bromate reduction driven by methane under oxygen-limiting  
16 condition. Long-term operational performance demonstrated that a complete bromate ( $\text{BrO}_3^-$ )  
17 reduction to bromide ( $\text{Br}^-$ ) could be achieved, with 100% of bromate removal efficiency  
18 under a volume loading of  $1 \text{ mg Br L}^{-1} \text{ d}^{-1}$ . Volatile fatty acids (VFAs) were produced in the  
19 reactor (ranging from 1.81 to 27.9 mg/L) under oxygen-limiting condition. High-throughput  
20 16S rRNA gene sequencing indicated that *Methanosarcina* became the only dominate  
21 methane-oxidizing microorganism and the abundance of *Dechloromonas* increased from 0.9%  
22 to 18.0% after feeding bromate. It is hypothesized that under oxygen-limiting conditions  
23 methane was oxidized into VFAs, which might be used to reduce bromate by dissimilatory

24 bromate-reducing bacteria (likely *Dechloromonas*). This study offers a potential technology  
25 for bromate removal by using the methane-based MBfR.

## 26 **Introduction**

27 Bromate ( $\text{BrO}_3^-$ ) contamination has been detected in various water environments, including  
28 drinking water, surface water and groundwater.<sup>1,2</sup> The occurrence of bromate contamination  
29 in drinking water or groundwater could pose serious threats to public health (e.g. kidney  
30 effects, nervous system effects and hearing loss under exposure of high bromate  
31 concentrations), as it has been classified as Group 2B carcinogen by World Health  
32 Organization,<sup>3</sup> thus attaching great significance to develop efficient bromate removal  
33 technologies.

34 Bromate removal from contaminated water could be achieved via physical (e.g. filtration and  
35 ultraviolet irradiation), chemical (e.g. coagulants and zero-valent iron) or biological  
36 processes.<sup>4</sup> Microbial bromate reduction has been proved to be one of the most effective  
37 processes for remediation of bromate-contaminated groundwater.<sup>1</sup> A variety of reactor  
38 configurations including biologically active carbon filters<sup>5</sup> and fixed-bed reactors<sup>6</sup> have been  
39 utilized for microbial bromate remediation. However, the supplement of external organic  
40 carbons (e.g. ethanol<sup>6</sup> or acetate<sup>7</sup>) as electron donors could potentially increase operational  
41 costs or incur a secondary pollution. Autotrophic bromate reduction using hydrogen as  
42 electron donor has also been demonstrated in hydrogen-based hollow fiber membrane biofilm  
43 reactors (MBfR).<sup>8,9</sup> Compared to hydrogen, methane is a much widely available carbon  
44 source,<sup>10</sup> thus could be as a promising electron donor for bromate removal. To date, various  
45 contaminants including nitrate, nitrite, chromate and perchlorate have been proved to be  
46 removable from synthetic groundwater or wastewater using methane-supported MBfR.<sup>11-13</sup>  
47 However, microbial bromate reduction driven by methane has not been reported so far.

48 Microbial methane oxidation can take place in both aerobic and anaerobic environments.  
49 Under aerobic conditions, methane is activated by methanotrophs through a mono-

50 oxygenation step, and organic intermediates such as methanol, acetate or formaldehyde is  
51 subsequently generated, providing electron and carbon sources for heterotrophic  
52 microorganisms.<sup>14, 15</sup> Recently, the aerobic methane oxidation process has been successfully  
53 applied to remove nitrate and chromate from wastewater through separated methane and  
54 oxygen supply.<sup>16, 17</sup> Under anaerobic conditions, methane oxidation is mediated by anaerobic  
55 methanotrophic archaea (known as ANME including ANME-1, ANME-2 and ANME-3).  
56 Previously, sulfate was the only confirmed electron acceptor for anaerobic methane oxidation  
57 process, in which a consortium of ANME archaea and sulfate reducing bacteria coupled  
58 methane oxidation to sulfate reduction.<sup>18</sup> Very recently, denitrifying anaerobic methane  
59 oxidation (DAMO) processes (nitrate or nitrite as electron acceptors) have been discovered.  
60 A novel member of ANME-2d lineage (*Candidatus* ‘Methanoperedens nitroreducens’,  
61 known as DAMO archaea) is able to oxidize methane by reverse methanogenesis, where  
62 methane is activated by methyl-coenzyme M reductase (MCR).<sup>19</sup> Moreover, *Candidatus*  
63 ‘Methylomirabilis oxyfera’ (known as DAMO bacteria) belonging to the NC10 phylum could  
64 oxidize methane through utilizing intracellular oxygen produced by the NO dismutation.<sup>20</sup> In  
65 recent studies, the DAMO processes have been successfully applied to remove nitrate from  
66 synthetic wastewater.<sup>11, 21</sup> Although aerobic or anaerobic methane oxidation processes have  
67 been proved practically useful in removing various contaminants, bromate removal driven by  
68 methane still remains unexplored regardless the presence of oxygen. Considering drinking or  
69 groundwater typically contains dissolved oxygen (DO, concentration up to 9 mg/L in a  
70 shallow groundwater),<sup>22</sup> methane oxidation under oxygen-limiting condition appears more  
71 practically feasible than anaerobic for bromate removal from contaminated drinking or  
72 groundwater.

73 The aim of this work is to explore the feasibility of bromate reduction using methane as  
74 electron donor under oxygen-limiting condition. A mixed culture enabling to couple bromate

75 reduction to methane oxidation was adopted and enriched by changing the feed of a lab-scale  
76 MBfR performing DAMO from nitrate to bromate. The reactor was initially inoculated with  
77 the enriched co-culture containing DAMO archaea and DAMO bacteria. After 250-day  
78 operation by feeding nitrate (start-up stage), synthetic groundwater containing bromate and  
79 dissolved oxygen was continuously fed to the reactor at hydraulic retention time of 1 day  
80 (operational stage for more than 100 days). Bromate removal rate was monitored to evaluate  
81 the reactor performance. The shift of microbial community was analysed based on high-  
82 throughput 16S rRNA gene sequencing.

83

## 84 **Materials and Methods**

### 85 *Reactor setup*

86 A laboratory-scale MBfR with 1 L working volume was set up in this study, as described  
87 previously.<sup>23</sup> Briefly, the reactor had eight bundles of composite hollow fibre membranes and  
88 membrane surface/reactor volume ratio was 181 m<sup>2</sup>/m<sup>3</sup>. The methane pressure inside all  
89 hollow fibres was controlled at 150 kPa using a gas-pressure regulator (Ross Brown,  
90 Australia). The bulk liquor in the MBfR system was mixed by a magnetic stirrer at 500 rpm  
91 (Labtek, Australia). A peristaltic pump (Masterflex, USA) and Tygon E-Lab tubing (internal  
92 diameter 3.1 mm, Masterflex, Cole-Parmer) was employed to recirculate the liquid at a flow  
93 rate of 100 mL/min. The MBfR was operated for about 360 days at 22±2 °C. The pH in the  
94 reactor was controlled between 7 and 8 by manual injection of 1 M NaOH.

### 95 *Operational conditions*

96 In order to obtain biofilm growth on the hollow fibre membranes, the MBfR was inoculated  
97 with 150 mL enriched co-culture dominated by DAMO archaea and DAMO bacteria.<sup>19</sup> Two  
98 stages, namely start-up (Stage I, 250 days) and operational stage (Stage II, 113 days), were

99 involved in the entire experimental period. In the start-up stage, nitrate stock solution (40 g  
100 N/L) was manually dosed into the reactor, giving an initial nitrate concentration of 40-160  
101 mg N/L after each dosage. During the operational stage, the influent (composition as shown  
102 in Supporting information) with a bromate concentration of ~1 mg Br/L was continuously fed  
103 into the reactor at hydraulic retention time (HRT) of 1 day. As nitrogen was not used to flush  
104 influent to remove oxygen, dissolved oxygen of 7-9 mg/L could be detected in influent.

105 Every week 3 liquid samples were regularly collected to monitor the bromate and bromide  
106 concentrations. In addition, volatile fatty acids (VFAs) in effluent were measured to monitor  
107 possible intermediates from methane oxidation under oxygen-limiting condition.

#### 108 *Analytical methods*

109 The effluent of 2 mL was sampled to determine the concentrations of bromate species and  
110 VFAs after 0.22  $\mu\text{m}$ -filtration. Bromate and bromide concentrations were measured by ion  
111 chromatography (Dionex ICS-2100).<sup>24</sup> A gas chromatography (7890A, Agilent) with a polar  
112 capillary column (DB-FFAP) and a flame ionisation detector (FID) was employed to  
113 determine VFAs. The pH level in the reactor was monitored by a pH meter (Oakton,  
114 Australia). DO concentration in influent was measured using a DO meter (HACH, USA).

115 For microbial community analysis, biofilm samples of 5 mL were collected from membrane  
116 surfaces at the end of start-up phase (Day 250) and on Day 335 of operational phase when a  
117 stable bromate removal efficiency was achieved. DNA was extracted from the biomass  
118 samples using the FastDNA SPIN for Soil kit (MP Biomedicals, USA) according to the  
119 manufacture's instruction. The 16S rRNA gene was amplified, sequenced and analyzed based  
120 on the procedures shown in Supporting Information.<sup>25</sup>

121

122

123

124 **Results and Discussion**125 *Performance of bromate bioreduction in the methane-based MBfR reactor*

126 In order to enrich biofilm for methane oxidation, 150 mL of inoculum harvested from a  
127 suspended reactor performing DAMO was seeded into the methane-based MBfR.<sup>19</sup> After the  
128 inoculation, nitrate was supplied in the liquid phase as the sole electron acceptor, while  
129 methane was delivered from the hollow fibre membranes as electron donor. A steady nitrate  
130 reduction rate of 3.7-5.0 mg N/L/d without nitrite accumulation was achieved at the end of  
131 start-up phase (Fig. S1). In parallel, a layer of biofilm gradually attached to the surface of  
132 hollow fiber membranes after 250 days of enrichment. On Day 251, the MBfR was switched  
133 into continuous operation feeding with synthetic contaminated water containing bromate and  
134 DO (7-9 mg/L), in order to test if microbial community shaped by nitrate feeding could  
135 reduce bromate under oxygen-limiting conditions. Interestingly, after switching electron  
136 acceptor from nitrate to bromate, the reactor achieved 100% of bromate removal efficiency  
137 (Fig. 1a). Purified nitrate reductase was previously reported to be potentially involved in  
138 bromate reduction process and denitrifying organisms also reduced bromate ( $\text{BrO}_3^-$ ) to  
139 bromide ( $\text{Br}^-$ ) after a complete nitrate reduction,<sup>26, 27</sup> indicating that some given  
140 microorganisms might be able to perform bromate reduction in the reactor after immediate  
141 switching of electron acceptor from nitrate to bromate. However, the removal percentage of  
142 bromate kept decreasing to 43% after 10 days. The possible reason is that microbial  
143 communities in the reactor were shifted after bromate introduction (see details later). The  
144 bromate removal efficiency was recovered to 66% on Day 274 and then 100% on Day 278,  
145 suggesting that biofilm community has eventually adapted to reduce bromate. The bromide  
146 concentration in effluent was stable at 0.8-1 mg/L during the whole experiment period (Fig.

147 1a), but other intermediates (e.g. bromite and hypobromite) were not detected, indicating that  
148 bromate in influent might be completely reduced to bromide.

149

#### 150 ***Production of VFAs by methane oxidation***

151 DO concentration of 7-9 mg/L in influent could be consumed by the biofilm, thus no DO  
152 could be detected in the MBfR during the entire Stage II, leaving the system a quasi-  
153 anaerobic condition (named as oxygen-limiting conditions in this study). Interestingly, VFAs  
154 were produced under oxygen-limiting conditions (Fig. 1b). During the initial 36 days of  
155 Stage II, total VFAs were much higher (22.2-27.9 mg/L), afterwards decreased to 1.81-13.6  
156 mg/L, possibly due to its ongoing consumption by microorganisms as carbon sources.  
157 Considering VFAs were not observed under anaerobic condition in Stage I, the oxygen  
158 introduction from the influent in Stage II could likely induce the VFAs production, which is  
159 consistent with our previous study.<sup>24</sup> In this study, total VFAs were dominated by acetate  
160 (>75%), followed by propionate (approximately 2-10%). Differently, previous studies  
161 documented that other soluble organic matters, e.g. methanol, formate, lactate, formaldehyde  
162 or citrate were dominant intermediates under micro-aerobic or aerobic conditions.<sup>28-30</sup>

163

#### 164 ***Microbial community structure shaped by bromate reduction***

165 The shift of microbial community structure under nitrate-feeding (Stage I) and bromate-  
166 feeding conditions (Stage II) was investigated based on 16S rRNA gene sequencing.  
167 Surprisingly, it was found that DAMO archaea and DAMO bacteria that dominated in the  
168 inoculum became relatively minor (< 1%) in the biofilm at the end of start-up phase, which  
169 explained the relatively slow nitrate removal rate (3.7-5.0 mg N/L/d) in Stage I compared to  
170 the seeding sludge reactor (average 25 mg N/L/d). A possible reason is that oxygen was

171 accidentally introduced into the reactor when replacing a recirculation tube on Day 150.  
172 Previous studies also reported that DAMO microorganisms are very sensitive to oxygen.<sup>31</sup>  
173 Compared to Stage I, the abundance of class *Methanomicrobia* and *Betaproteobacteria* in the  
174 biofilm, significantly increased from 0.62% to 5.2% and from 11.2% to 22.9%, respectively  
175 at the end of Stage II (Fig. 2). Further analysis of the community composition at the genus  
176 level indicated that the class of *Methanomicrobia* and *Betaproteobacteria* were dominated by  
177 the genus of *Methanosarcina* and *Dechloromonas*, respectively. In comparison with the  
178 biofilm of Stage I, the abundance of *Methanosarcina* increased from 0.18% to 4.0% and  
179 became the only dominating methane-related archaea in bromate-shaped biofilm. In addition,  
180 the abundance of *Dechloromonas* increased significantly from 0.9% to 18.0% after bromate  
181 was supplied as the only electron acceptor, indicating *Dechloromonas* was potentially  
182 responsible for bromate reduction using VFAs as carbon and electron sources.

183

#### 184 ***Mechanisms of bromate reduction coupled to methane oxidation***

185 It has been reported that nitrate, nitrite, perchlorate and chromate could be reduced by using  
186 methane as sole electron donor in CH<sub>4</sub>-based MBfRs.<sup>12, 13, 32</sup> To the best of our knowledge,  
187 this study is the first report that a complete bromate reduction could also be achieved in the  
188 methane-based MBfR. The bromate removal seems to be achieved via synergistic  
189 interactions between multiple microorganisms. In order to elucidate bromate reduction driven  
190 by methane under oxygen-limiting conditions, two batch tests were conducted at the end of  
191 Stage II (Supporting information). In the first abiotic control without microorganisms, no  
192 bromate was reduced with methane and fresh medium (Fig. S2), ruling out the possibility of  
193 bromate reduction via chemical reactions. In the second test without methane supply for the  
194 reactor, no bromate reduction and bromide production could be observed as well (Fig. S2),

195 indicating methane plays an important role in the bromate reduction process in the MBfR. It  
196 is assumed methane was partially oxidized to VFAs under oxygen-limiting conditions, in  
197 terms of the fact that methane was the only carbon source fed to this reactor. The VFA  
198 production was likely through aerobic methane oxidation, although aerobic methanotrophs  
199 were not identified by 16S rRNA gene sequencing. Interestingly, *Methanosarcina*, as a  
200 known methanogen, became the only methane-related microorganism. It has been reported  
201 that *Methanosarcina barkeri* could mediate methane oxidation and produce methanol and  
202 acetate as oxidation product,<sup>33</sup> indicating *Methanosarcina* is probably responsible for VFA  
203 production in Stage II. Simultaneously, *Dechloromonas*, whose abundance increased by 17%  
204 after the input of bromate, might play a role in utilizing VFAs as electron donor to reduce  
205 bromate. It has been documented that *Dechloromonas* is able to reduce chlorate, perchlorate  
206 or nitrate using acetate as electron donor.<sup>34</sup> The perchlorate reducing bacterium  
207 *Dechloromonas* sp. PC1 was also reported to reduce bromate without measurable growth.<sup>35</sup>  
208 In addition, bromate was reduced to bromide via mediation of nitrate reductase in  
209 denitrifying *Pseudomonas* spp.<sup>36</sup> Given that nitrate was not provided in Stage II, unique  
210 conditions (e.g. oxygen-limiting and only bromate fed as electron acceptor) in the MBfR  
211 might select a specialized bromate-reducing bacterium, which warrants further studies. Based  
212 on long-term performance, batch tests and microbial community structure results, a  
213 hypothesis was proposed for the bromate reduction in the methane-based MBfR (Fig. 3). It is  
214 assumed methane was oxidized into VFAs by *Methanosarcina* or unknown methanotrophs  
215 under oxygen-limiting conditions, then the generated VFAs served as electron donors for  
216 dissimilatory bromate-reducing bacteria (like *Dechloromonas*). The detailed pathway and the  
217 responsible microorganisms should be elucidated by isotope, metagenomics and  
218 metatranscriptomics in the future.

### 219 ***Practical implications***

220 This study provided the first proof of concept that the complete bromate removal is feasible  
221 in the methane-based MBfR under oxygen-limiting conditions. A bromate removal rate of 1  
222 mg Br L<sup>-1</sup> d<sup>-1</sup> (5.5 mg/m<sup>2</sup>/d) was achieved in this work. Compared to the reported rates (Table  
223 S1), bromate removal rate achieved in this work is lower than the typical rate in hydrogen-  
224 based MBfR (15.6-232 mg/m<sup>2</sup>/d), while it is comparable to the rates achieved in reactors  
225 using ethanol (0.4-1.0 mg/L/d) or glucose as carbon source (1.5-3.0 mg/m<sup>2</sup>/d). The reactor  
226 operation should be further optimized to increase the bromate removal rate by regulating  
227 operation conditions, e.g. methane partial pressure and oxygen flux rates. In addition, high  
228 nitrate concentrations are commonly expected in most groundwater<sup>37</sup> and may inhibit  
229 bromate removal as nitrate and bromate are competing terminal electron acceptors.<sup>38</sup> The  
230 effect of nitrate on bromate removal efficiency remains further exploration.

231 Although the bromate removal rate achieved in this study is relatively limited, methane  
232 supported bromate removal technique might be an alternative process in bromate-containing  
233 water treatment as it has several advantages over other technologies. Firstly, methane is  
234 inexpensive and widely available compared to organic carbon sources (e.g. methanol) or  
235 hydrogen. In addition, residue organic matter could be detected in effluent to cause secondary  
236 pollution due to excess addition of soluble organic carbon, while methane solubility is much  
237 lower and will not remain in effluent. Furthermore, for aerobic methane oxidation, great  
238 potential safety hazard could be involved when mixing flammable methane with oxygen in  
239 membrane lumens. The MBfR configurations used in this study, in which methane is  
240 supplied through membranes and oxygen is provided via liquid, avoids the safety hazard.

241

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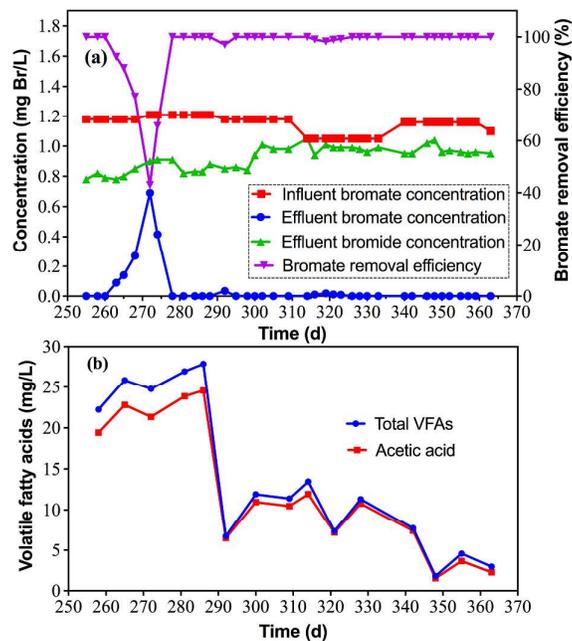
248 **Supporting Information Available:** Additional method details and supporting data, results  
249 in figures and tables.

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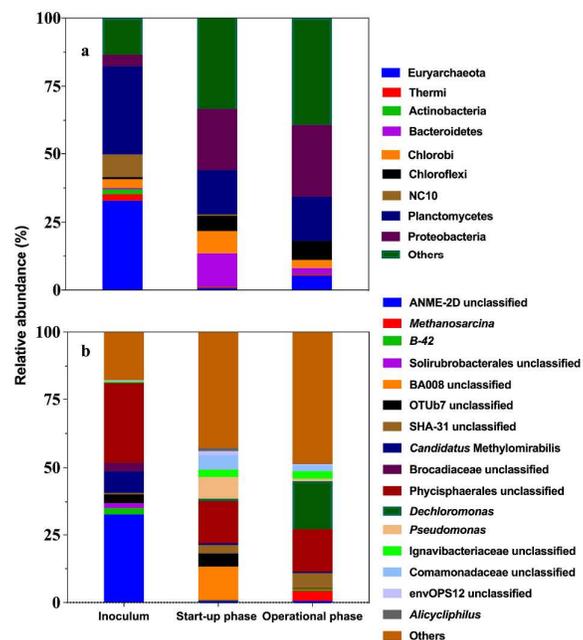


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349 Fig. 1 Long-term performance of bromate reduction during Stage II in the MBfR (a) and  
350 variations of residual volatile fatty acids (VFA) produced in the reactor (b) under oxygen-  
351 limiting conditions (Stage II).

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355 Fig. 2 Relative abundances of microbial communities at different stages: (a) phylum, and (b)

356 genus. The relative abundance is defined as a percentage in total microbial sequences in a

357 sample. Phylum or genera that account for  $\geq 1\%$  of at least one 16S rRNA gene sequence are

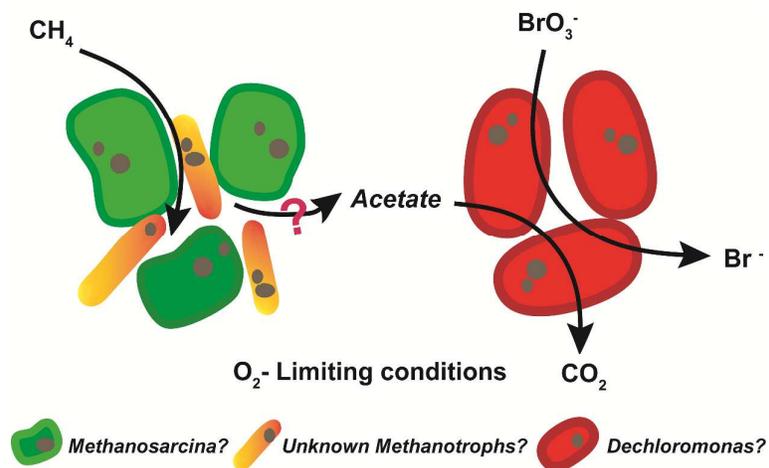
358 shown, while phylum or genera with an abundance of less than 1% in all sequences are

359 grouped into Others.

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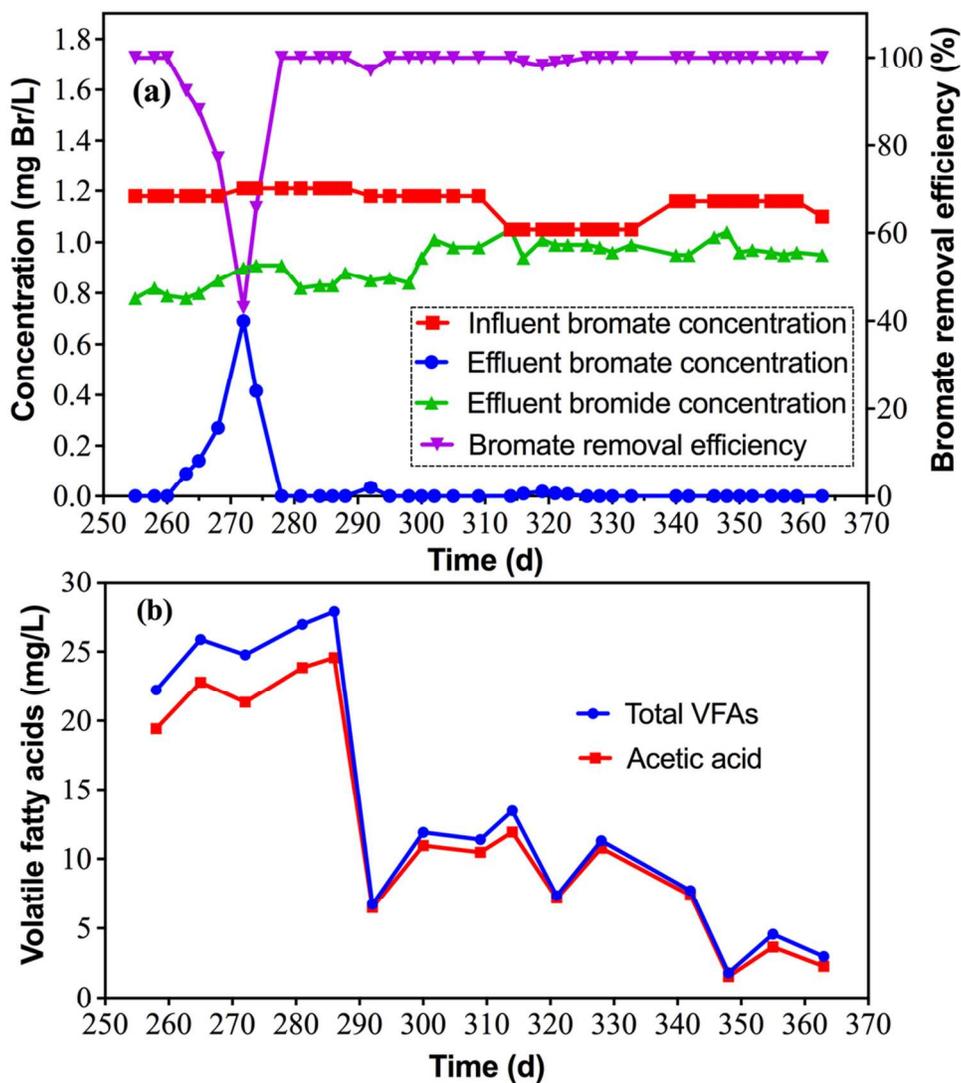


Fig. 1 Long-term performance of bromate reduction during Stage II in the MBfR (a) and variations of residual volatile fatty acids (VFA) produced in the reactor (b) under oxygen-limiting conditions (Stage II).

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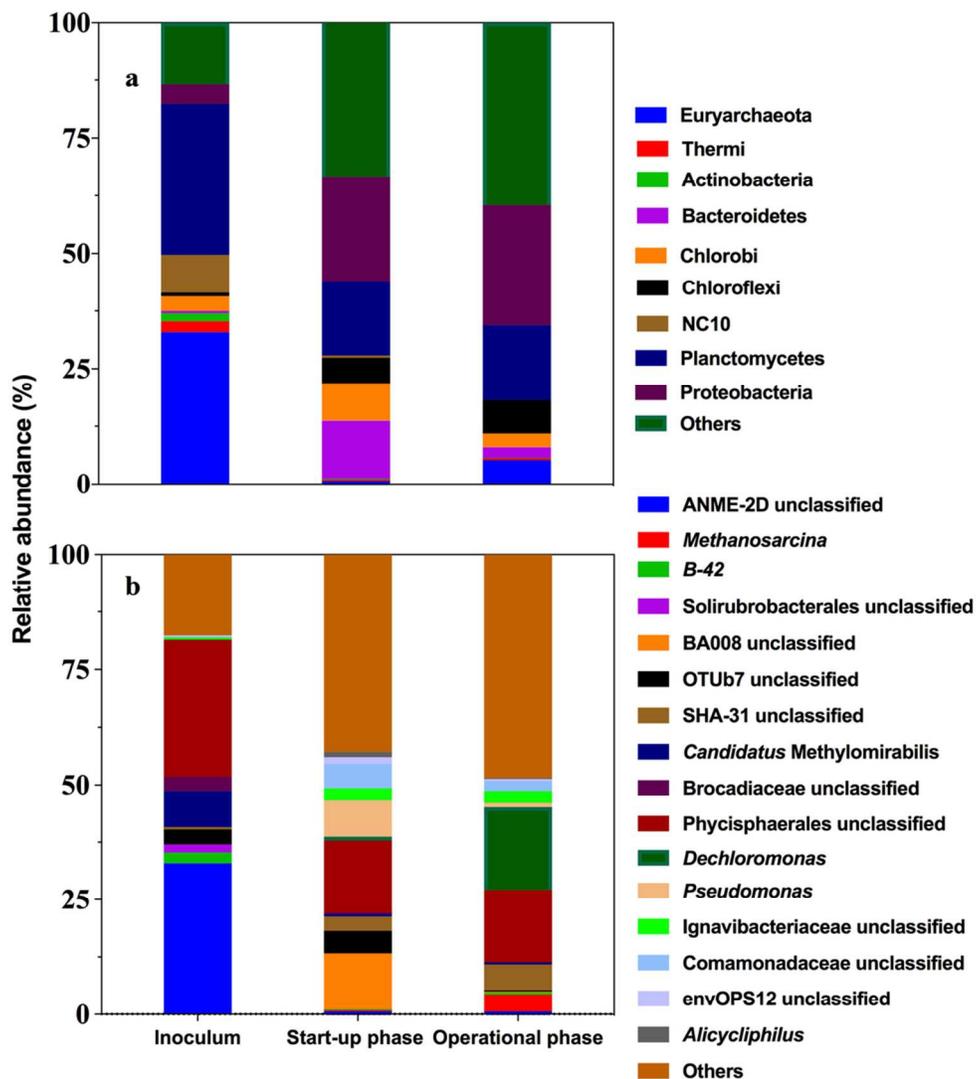


Fig. 2 Relative abundances of microbial communities at different stages: (a) phylum, and (b) genus. The relative abundance is defined as a percentage in total microbial sequences in a sample. Phylum or genera that account for  $\geq 1\%$  of at least one 16S rRNA gene sequence are shown, while phylum or genera with an abundance of less than 1% in all sequences are grouped into Others.

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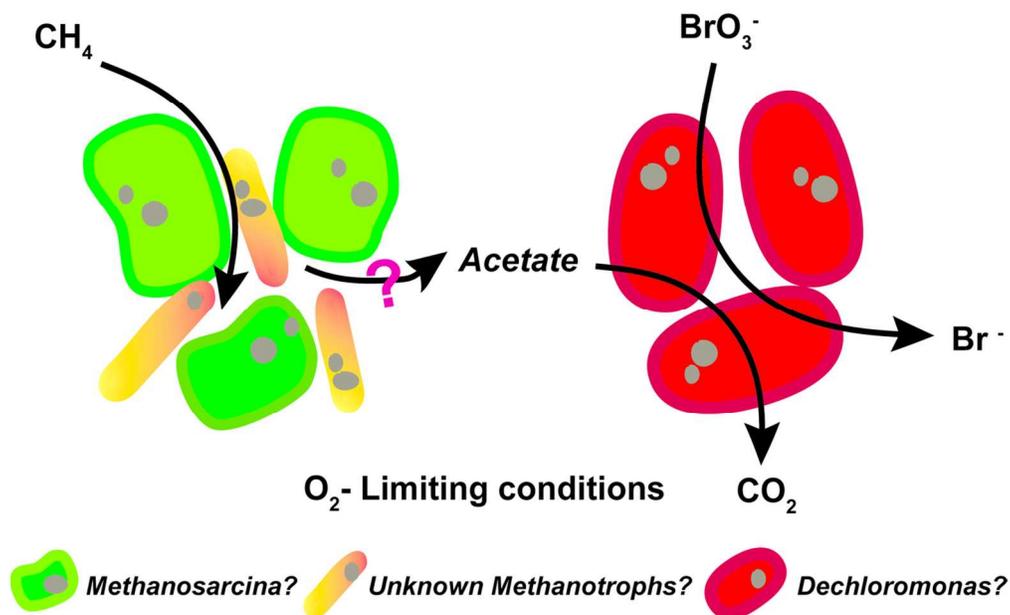
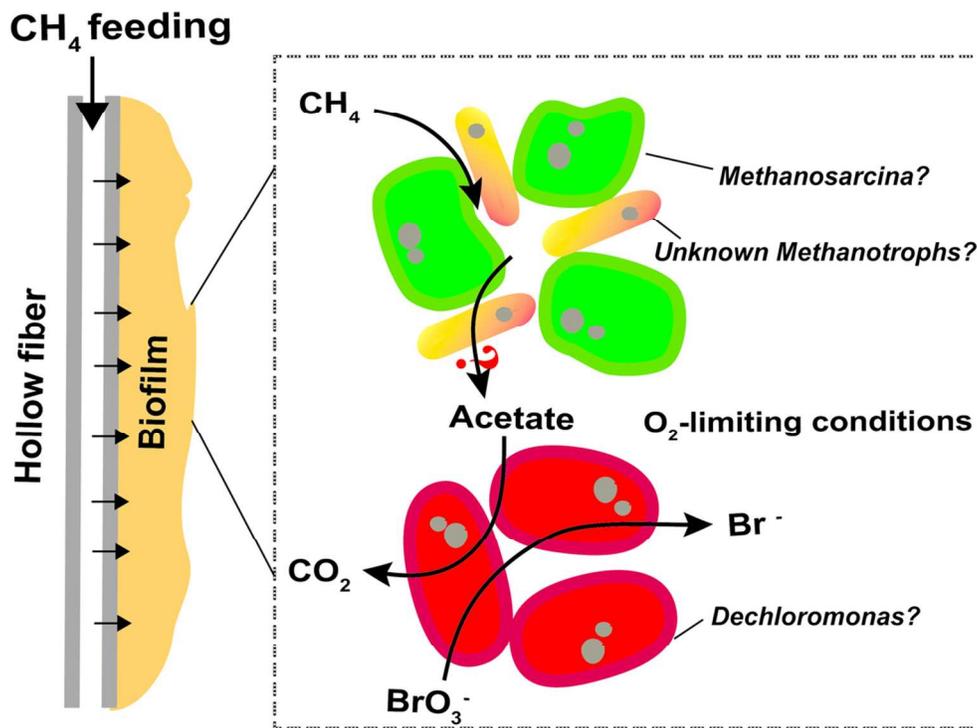


Fig. 3 The proposed pathway of bromate reduction coupled to methane oxidation under oxygen-limiting conditions. Methanosarcina or unknown methanotrophs might convert methane into VFAs under oxygen-limiting conditions, and then the produced VFAs would be utilized by potential bromate reducers (e.g. Dechloromonas) to reduce bromate into bromide.

119x74mm (300 x 300 DPI)



102x76mm (300 x 300 DPI)